EAST Search History

Ref #	Hits	Search Query	DBs	Default Operator	Plurals	Time Stamp
S1	1	hydrocarbon with (distilation adj3 column)	US-PGPUB; USPAT; USOCR; EPO; JPO; DERWENT; IBM_TDB	OR	ON	2006/10/26 11:17
S2	2831	hydrocarbon with (distillation adj3 column)	US-PGPUB; USPAT; USOCR; EPO; JPO; DERWENT; IBM_TDB	OR	ON	2006/10/26 11:18
S3	103	hydrocarbon adj distillation adj3 column	US-PGPUB; USPAT; USOCR; EPO; JPO; DERWENT; IBM_TDB	OR	ON	2006/10/26 11:19
S4	97	hydrocarbon adj distillation adj column	US-PGPUB; USPAT; USOCR; EPO; JPO; DERWENT; IBM_TDB	OR	ON	2006/10/26 11:18
S5	4	S4 and simulation	US-PGPUB; USPAT; USOCR; EPO; JPO; DERWENT; IBM_TDB	OR	ON	2006/10/26 11:18
S6	341	(hydrocarbon with (distillation adj3 column)) and simulat$4	US-PGPUB; USPAT; USOCR; EPO; JPO; DERWENT; IBM_TDB	OR	ON	2006/10/26 11:27
S7	19	(hydrocarbon with (distillation adj3 column)) same simulat$4	US-PGPUB; USPAT; USOCR; EPO; JPO; DERWENT; IBM_TDB	OR	ON	2006/10/26 11:23
S8	0	S6 and lumping	US-PGPUB; USPAT; USOCR; EPO; JPO; DERWENT; IBM_TDB	OR	ON	2006/10/26 11:23

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S9	41	S6 and lump$5	US-PGPUB; USPAT; USOCR; EPO; JPO; DERWENT; IBM_TDB	OR	ON	2006/10/26 11:26
S10	15	(lumping adj3 method)	US-PGPUB; USPAT; USOCR; EPO; JPO; DERWENT; IBM_TDB	OR	ON	2006/10/26 11:26
S11	181	S6 not S9	USPAT	OR	OFF	2006/10/26 11:27
S12	4	S11 and constituents and (material with balance)	USPAT	OR	ON	2006/10/26 11:28

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90% **Simulation of Compositional Processes: The Use of Pseudocomponents in Equation-of-State Calculations**

SPE eLibrary The accuracy of the method is demonstrated by comparing phase splits, lumped mole fractions in liquid and vapor phases, and phase densities and phase viscosities obtained from a lumped fluid description with the same data as those obtained from a fully compositional description of hydrocarbon systems. Let us now c$msider a lumped description of then ~- component system in terms of ng groups, n~bered S, t. 11) i., To handle the minimization problem, we choose as vari- ables the liquid mole numbers, np,h=xpsfL, s=l.

90% **Reliable Wax Predictions for Flow Assurance**

SPE eLibrary The recently developed model of Coutinho is, however, based on high accuracy thermodynamic data. In order to put wax calculations on a firmer footing, Coutinho and co-workers have developed a wax model that is directly based on high-quality laboratory data for the properties of liquid and solid hydrocarbons and their mixtures [9,10 We believe that this behaviour is an artifact of the lumped model. Lumping the non-n-paraffins has virtually no effect on the wax calculations.

89% **Prediction of CO2/Crude Oil Phase Behavior Using Supercritical Fluid Chromatography**

SPE eLibrary Some uncertainty inevitably arises from the lumping of real compo- nents into Paeudocomponents, however, because the parameters required for EOS calculations (Pc, T., w, 6) cannot be measured directly. In order to estimate 6's using SFC, an equation is needed that relates the SFC e}ution-time of a hydrocarbon to its VIntry inter- action parameter with the CO? carrier fluid, One such equation is derived as follows.

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- Try different keywords.
- Try more general keywords.
- Try fewer keywords.
- Try your query on the entire web.

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83% **Obtaining PVT Data For Very Sour Retrograde Condensate Gas and Volatile Oil Reservoirs: A Multi-disciplinary Approach**

SPE eLibrary Finally, to obtain good matches on liquid densities, volume shifts on the heavier components was the third targeted tuning factor(s). This was dooe by assigning properties to the heaviest component which corresponded to progressively higher molecular weight pseudo components. Most of the lumping schemes suggested for developing pseudo components usually pick a carbon number that it closer to the smaller end of the range. Therefore, the second or third lowest carbon number component in a pseudo component range, is usually considered the best average.

82% **Simulation of Gas Condensate Reservoir Performance**

SPE eLibrary This paper presents a pseu- doization procedure that reduces the multicomponent con- densate fluid to a pseudo two-component mixture of surface gas and oil. We can think of pseudoization in terms of either lump- ing components or combining streams. The Mixture z might be flashed at a low pressure and temperature with liquid and gas separator products resulting. In lumping components, each psendocomponent con- sists of a subset of the original n components, and none of the members of this subset are pr~ent in my of the other pseudocomponents.

82% **Predicting Retrograde Phenomena and Miscibility Using Equation of State**

SPE eLibrary ondensation and condensing-gas-drive recovery to achieve dynamic miscible diaplaeement or multiple phenomena have important applications in NGL production and contact miscible displacernen In Table I the mixing rules for these parameters are based on different conformal solution theories of mixtures. An ec aation of state, such as Equation 1 with a choice of mixing rules is based on binary interactions. The parameters Ati, bfi, and Cii of this equation of state are derived from pm component properties while parameters Aij, bijt nd Ci. are derived from binary data of i and j.

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